## IN THE CLAIMS

The following claim set replaces all prior versions, and listings, of claims in the application:

- (currently amended) A continuous process for preparing caprolactam in a multistage by Beckmann rearrangement of cyclohexanone oxime, said process comprising
  - a) feeding (i) oleum and (ii) cyclohexanone oxime into a first stage reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>,
  - feeding (iii) a portion of the first <u>stage</u> reaction mixture and (iv) cyclohexanone oxime into a second <u>stage</u> reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>, <u>and</u>
  - c) withdrawing a portion of the second <u>stage</u> reaction mixture, wherein the process further comprises obtaining the cyclohexanone oxime that is fed to the <u>first and second stage</u> reaction mixtures <u>and is containing less than</u> 1 wt.% water by:
    - preparing an organic medium comprising cyclohexanone oxime dissolved in an organic solvent
    - separating, by distillation, cyclohexanone oxime from said organic medium.
- (currently amended) A process according to claim 1, said process further comprising
  - feeding (v) a portion of the second <u>stage</u> reaction mixture and (vi) cyclohexanone oxime into a third <u>stage</u> reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>, and
  - e) withdrawing a portion of the third stage reaction mixture.

(currently amended) Process according elaim 1 claim 2, wherein the
cyclohexanone oxime that is fed to the third stage reaction mixtures contains less
than 1 wt.% water.

## (canceled)

- (currently amended) Process according to claim 1, wherein the SO<sub>3</sub> content of the <u>first and second stage</u> reaction mixtures comprising caprolactam, sulfuric acid and SO<sub>3</sub> is at least 6 wt.%.
- (currently amended) Process according to claim 1, wherein the SO<sub>3</sub> content of the <u>first and second stage</u> reaction mixtures comprising caprolactam, sulfuric acid and SO<sub>3</sub> is at least 8 wt.%.
- (currently amended) Process according to claim 1, wherein the SO<sub>3</sub> content of the <u>first and second stage</u> reaction mixtures comprising caprolactam, sulfuric acid and SO<sub>3</sub> is at least 10 wt.%.
- (previously presented) Process according to claim 1, wherein the SO<sub>3</sub> content of the oleum is between 18 and 35 wt %
- (currently amended) Process according to claim 1, wherein the process comprising comprises:
  - a) feeding (i) oleum and (ii) cyclohexanone oxime into a the first stage reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>,
  - b) feeding (iii) a portion of the first stage reaction mixture and (iv) cyclohexanone oxime into a second stage reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>, wherein the molar ratio M of the second reaction mixture is between 1.0 and 1.4 and the SO<sub>3</sub> content of the second stage reaction mixture is higher than 6 wt.%, and

- withdrawing a portion of the second reaction mixture from which caprolactam is recovered.
- (currently amended) Process according to claim 9, wherein the SO<sub>3</sub> content of the second stage reaction mixture is higher than 8 wt.%.
- (currently amended) Process according to claim 9, wherein the SO<sub>3</sub> content of the second stage reaction mixture is higher than 10 wt.%.
- (currently amended) Process according to claim 1, wherein the process comprising
  - a) feeding (i) oleum and (ii) cyclohexanone oxime into e the first reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>,
  - feeding (iii) a portion of the first <u>stage</u> reaction mixture and (iv) cyclohexanone oxime into a second <u>stage</u> reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>.
  - withdrawing a portion of the second <u>stage</u> reaction mixture;
  - d) feeding (v) a portion of the second <u>stage</u> reaction mixture and (vi) cyclohexanone oxime into a third <u>stage</u> reaction mixture comprising caprolactam, sulfuric acid and SO<sub>3</sub>, wherein the molar ratio M of the third <u>stage</u> reaction mixture is between 1.0 and 1.4 and the SO<sub>3</sub> content of the third <u>stage</u> reaction mixture is higher than 6 wt.%, <u>and</u>
  - withdrawing a portion of the third <u>stage</u> reaction mixture from which caprolactam is recovered.
- (currently amended) Process according to claim 12, wherein the SO<sub>3</sub> content of the third <u>stage</u> reaction mixture is higher than 8 wt.%.
- (currently amended) Process according to claim 12, wherein the SO<sub>3</sub> content of the third <u>stage</u> reaction mixture is higher than 10 wt.%.

- 15. (new) Process according to claim 12, wherein the cyclohexanone oxime that is fed to the first, second and third stage reaction mixtures and contains less than 1 wt.% water is obtained by:
  - preparing an organic medium comprising cyclohexanone oxime dissolved in an organic solvent; and
  - separating, by distillation, cyclohexanone oxime from said organic medium.
- (new) Process according to claim 15, wherein the cyclohexanone oxime that is fed to the first, second and third stage reaction mixtures contains less than 0.2 wt % water
- (new) Process according to claim 15, wherein the cyclohexanone oxime that is fed to the first, second and third stage reaction mixtures contains less than 0.1 wt.% water.
- (new) Process according to claim 1, wherein the cyclohexanone oxime that is fed to the first, second and third stage reaction mixtures contains less than 0.2 wt.% water.
- (new) Process according to claim 1, wherein the cyclohexanone oxime that is fed to the first, second and third stage reaction mixtures contains less than 0.1 wt.% water.